



Assessment of biomethane production from maritime common reed

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Aim

1. To perform an energy balance of the system
2. Quantify GHG emissions in comparison with a fossil reference system
3. Estimate net nutrient recirculation potential

Case study Kalmar



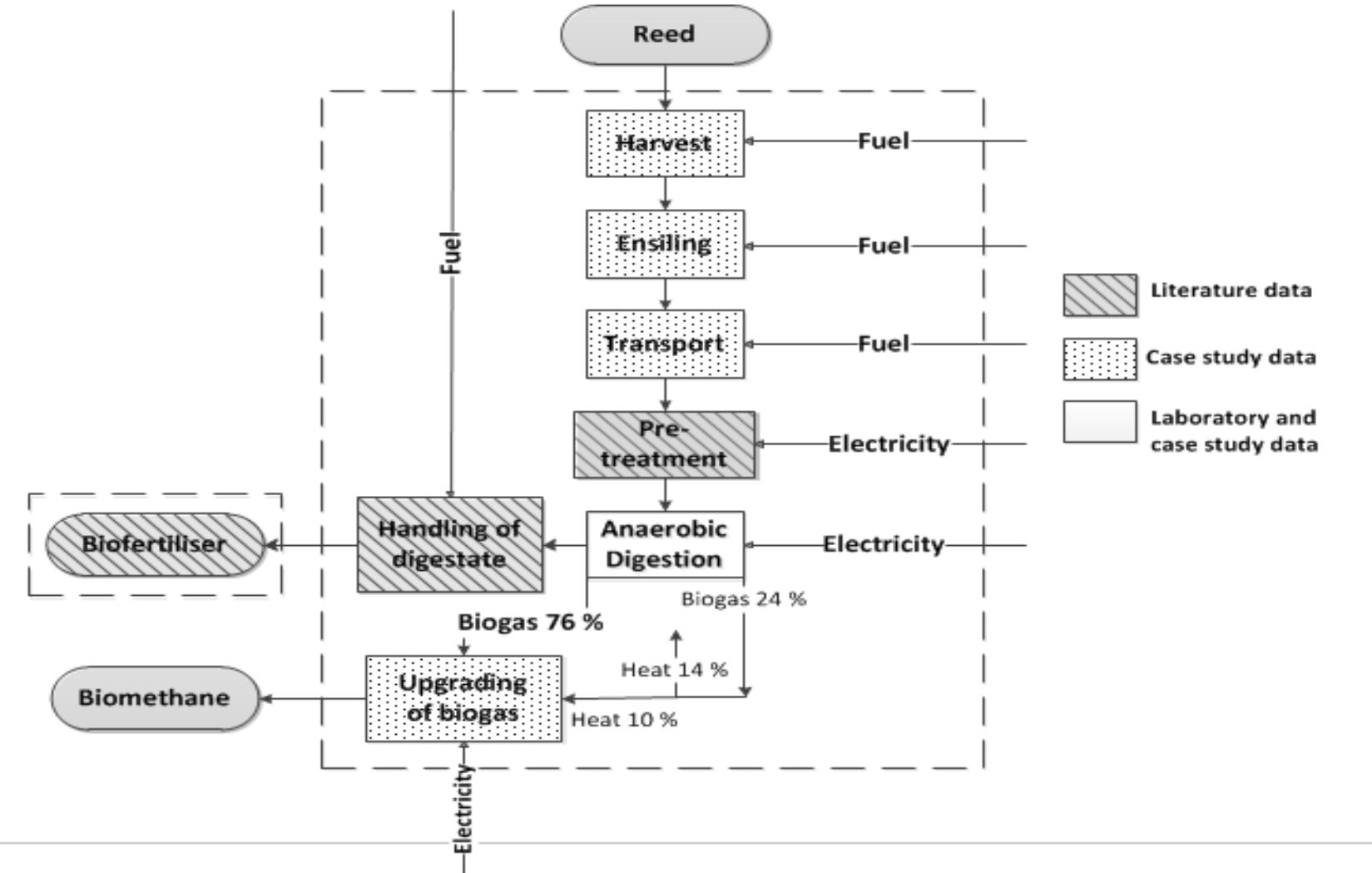
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Harvesting



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System description



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System analysis

1. Energy analysis

- Energy input
- Methane yield
- Net production

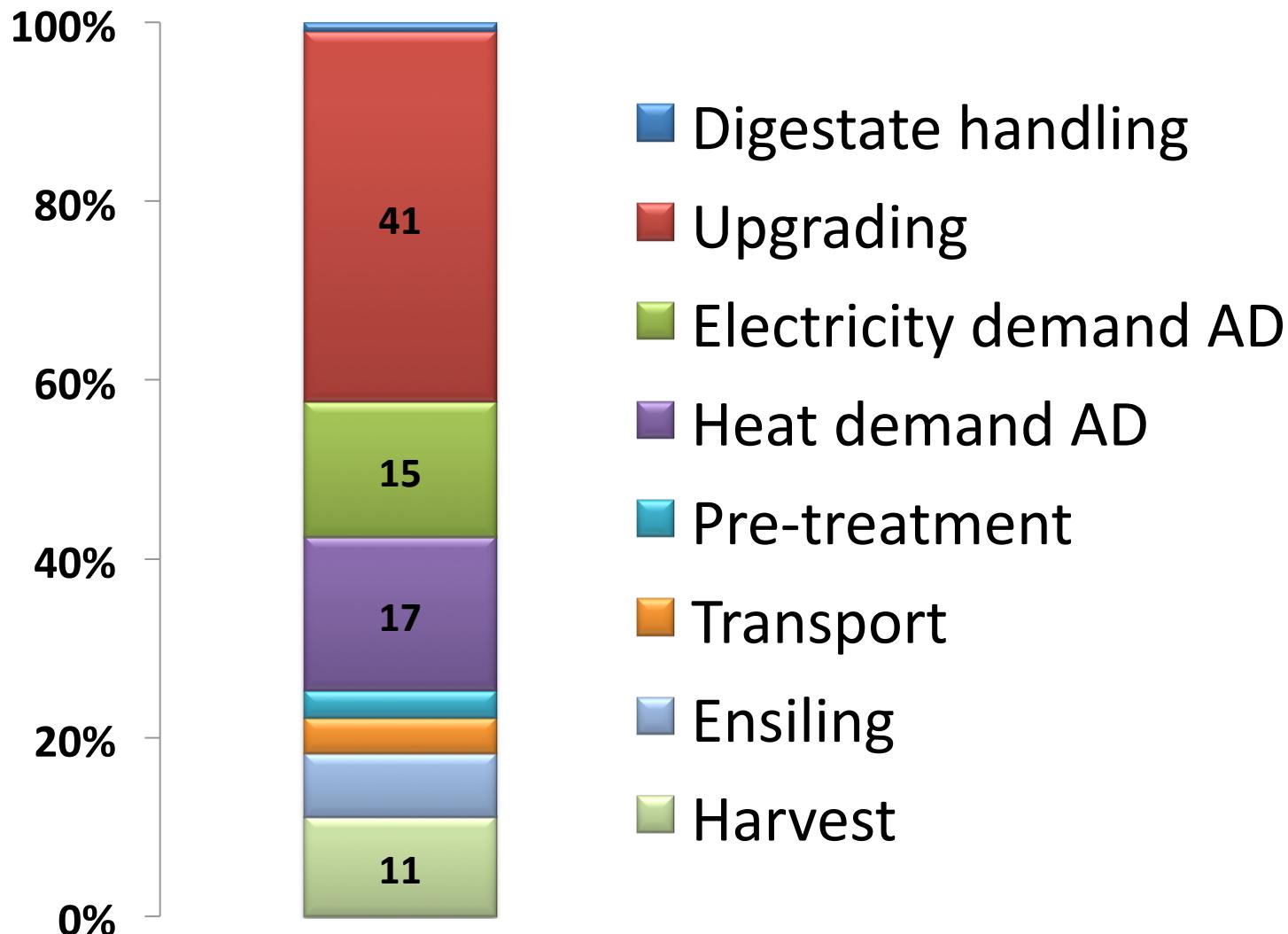
2. Greenhouse gas emissions

3. Nutrient retrieval



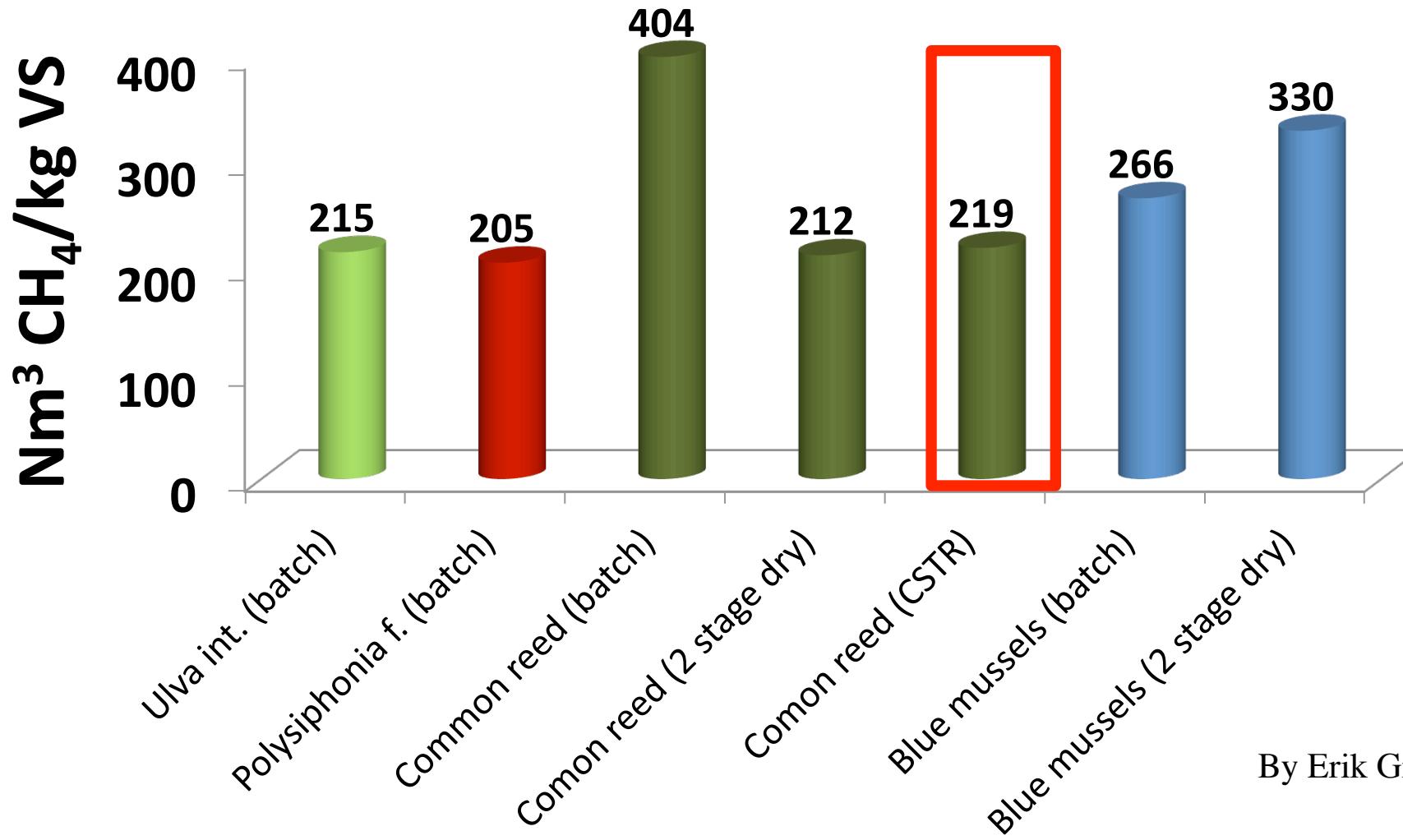
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Results energy input



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Results methane yield



By Erik Gregeby

Results Energy analysis

- The energy demand of the system corresponds to 40% of the biomethane produced
- Net production is approximately 40 L gasoline-equivalents per t of reed
- About 50% of support energy is from renewable resources
- A hypothetical harvest of all reed in the Kalmar Municipality (180 ha) corresponds to less than 1% of the total energy utilisation of the transport sector

Results GHG emissions

- A reduction of 80% in comparison with a fossil reference system is possible



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Results Net nutrient flows

- Almost all of the retrieved P can be recirculated to farm land
- Approximately 60% of the retrieved N can be recirculated to farm land



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Results Net nutrient flows

- A hypothetical harvest of the total reed area in Kalmar County (ca. 530 ha) corresponds to:
- 1 % of annual N leackage from farm land
- 20 % of annual P leackage form farm land

Summary 1

- Positive energy balance
- Satisfactory reduction of GHG emissions
- Possibility to recirculate nutrients
- System design and system boundaries are key factors for our results

Summary 2

Further studies are necessary

- Socio-economic aspects of biomass retrieval
- Ecological risks with large scale harvest



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Thank you for listening!



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Thank you for paying!



Forskningsrådet Formas

Formas främjar framstående forskning för hållbar utveckling



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Energy analysis

- Primary energy
- Several indicators e.g. Input/Output

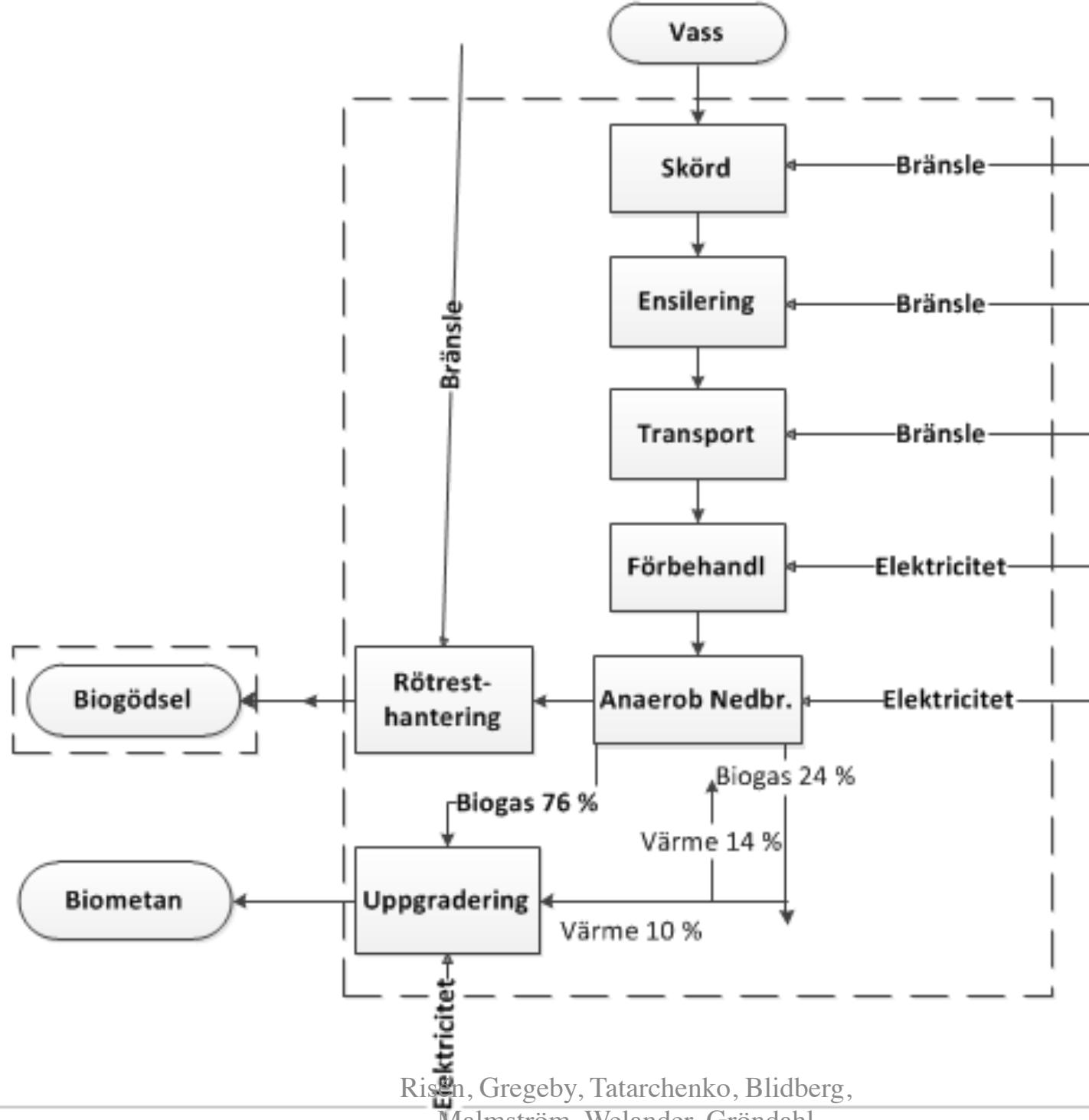


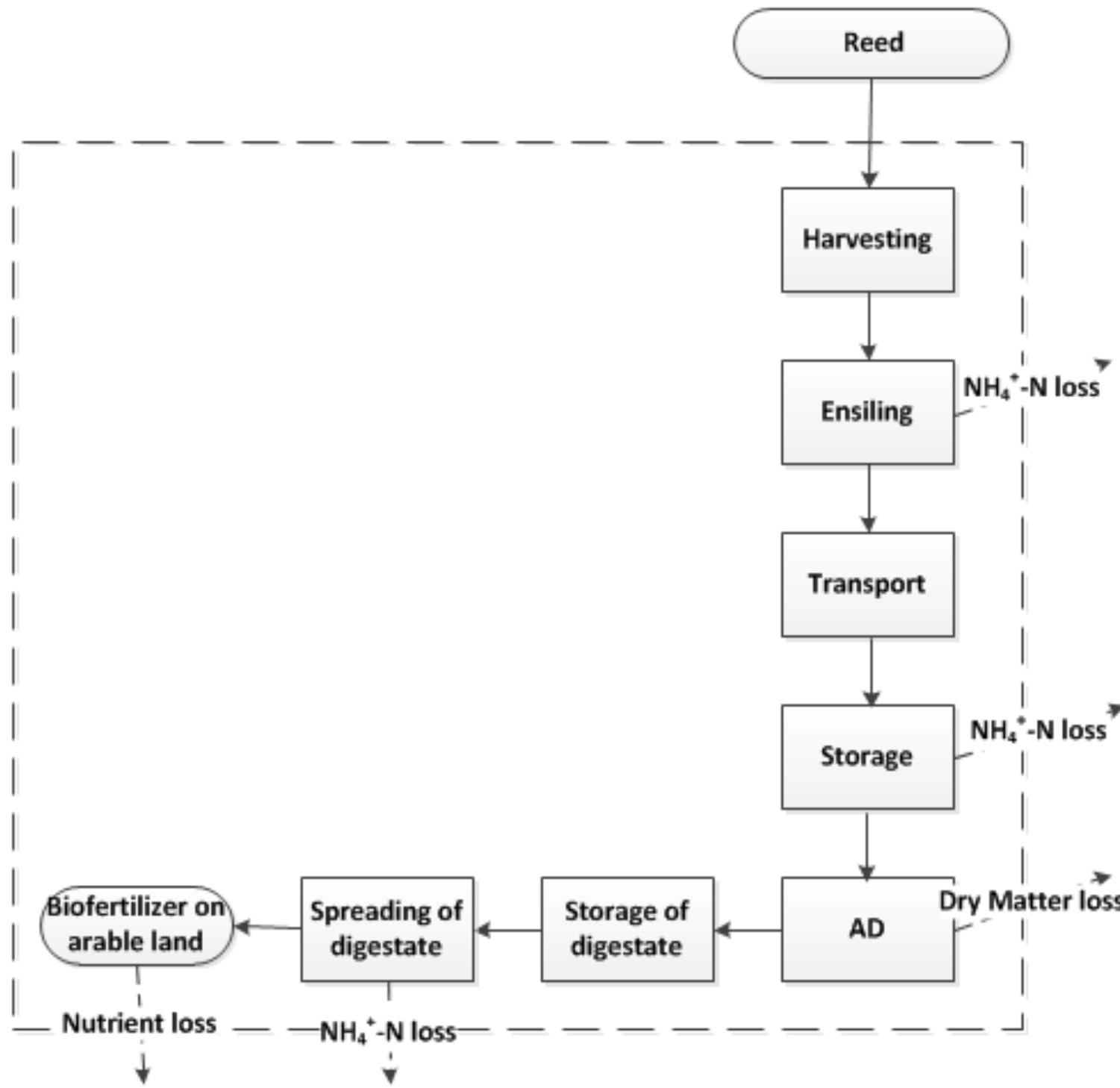
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Net nutrient flows

Reed composition

Reed composition	Average (% of DM)
DM	44.6 (% of dwt)
VS	93.8
TKN	1.5
P	0.14
K	1.2





Energibalans

$$IOR = \frac{(E_{\text{tot in}} - E_{\text{subst}})}{E_{\text{tot out}}}$$

$$NEV = E_{\text{tot out}} + E_{\text{subst}} - E_{\text{tot in}}$$

$$\text{ERenEF} = \frac{E_{\text{tot out}} - E_{\text{nrin}}}{E_{\text{tot out}}}$$

Table 3.1 Primary energy input into harvesting, ensiling, pre-treatment, transportation and spreading of digestate.

Process step	Reed		Straw		
	This study	Hansson and Fredriksson, 2004	Pöschl et al., 2010	Berglund and Börjesson, 2006	Börjesson and Berglund, 2006
Harvesting (MJ/tonne dwt)	559		n.a.	280 ^A	230 ^B
Ensiling (MJ/tonne dwt)	332		140 ^C	n.a.	n.a.
Transportation (MJ/tonne dwt, km) (tractor/truck/digestate tank truck)	8.5/12.8/ 4.2	4.4/n.a./ n.a.	6.9/n.a./ 2.5	n.a./3.5 ^D / n.a.	n.a./3.5 ^D / n.a.
Pre-treatment (MJ/tonne dwt)	150		n.a.	n.a.	33
Spreading of digestate (MJ/tonne dwt)	150	400 ^E	202 ^E	170 ^E	250 ^E

^A Straw recovery and transport from field to storage

^B Diesel consumption by machinery + manufacture of transport machinery

^C Fuel consumption during baling operations

^D Calculated from 2.0 MJ/t wwt with an DM content of 82 %

^E Calculated from an DM content of 10 % in the digestate

Table 3.2
Primary energy input biogas plant operation and biogas upgrading

Process step	<u>Biogas plant operation and biogas upgrading</u>		
	This study	Berglund and Börjesson, 2006	Beil, 2009
Biogas plant heat (MJ/m ³ substrate, 10 % DM)	285 ^A	110 ^B	n.a.
Biogas plant electricity (MJ/m ³ substrate, 10 % DM)	151	66	n.a.
Biogas upgrading heat (MJ/Nm ³ biogas) ^C	4.2 (764*)	n.a.	2.1
Biogas upgrading electricity (MJ/Nm ³ biogas)	0.8 (137*)	n.a.	0.9

^A Large-scale biogas plant (CSTR, thermophilic process temperature)

^B Large-scale biogas plant (CSTR, mesophilic process temperature)

^C Chemical (amine) absorption

* MJ/m³ substrate, based on the biogas production from 1 tonne wwt of reed (1tonne wwt = 1 m³ substrate)

n.a.-Not Available

Table 2.2 Energy indicators

Indicator	Acronym	Equation	Measure	Previous use
Input output ratio	IOR	$IOR = \frac{E_{tot\ in} - E_{subst}}{E_{tot\ out}}$	Energy efficiency of a system IOR ratio < 1 positive	(Berglund and Börjesson, 2006; Börjesson et al., 2010; Pöschl et al., 2010)
Net energy value	NEV	$NEV = E_{tot\ out} + E_{subst} - E_{tot\ in}$	Net energy output from the system NEV>0 positive	(Hansson and Fredriksson, 2004; Varadharajan et al., 2008)
Net renewable energy value	NREV	$NREV = E_{tot\ out} + E_{subst} - E_{Nrin}$	Amount of avoided non renewable energy usage NREV>0 positive	(Graboski, 2002; von Blottnitz H. and Curran, 2007; Varadharajan et al., 2008)
Non renewable input ratio	NRIR	$NRIR^A = \frac{E_{Nrin}}{E_{tot\ in}} * 100$	Percentage of total energy input of non renewable origin	Not previously used
Energy Renewability Efficiency	ERenEF	$ERenEF = \frac{E_{tot\ out} - E_{nrin}}{E_{tot\ out}} * 100$	Renewability Efficiency	(Malca and Freire, 2006)

^A Heating of the plant with biogas was considered as an external energy input in NRIR in order to assess all energy utilised.

Results energy indicators

Table 3.5 Input Output Ratio, Net Energy Value, Net Renewable Energy Value, Net Renewable Input Ratio and Energy Renewability Efficiency applied to the case study system. Criteria for indicators to be positive are shown in brackets.

IOR (<1)	NEV [MJ/ t wwt] (>0)	NREV [MJ/ t wwt] (>0)	NRIR [%]	ERenEF
0.39	1 644	1 891	53 %	68 %

Växthusgasindikator

$$I = \frac{CO_2 \text{ eq tot } g - CO_2 \text{ eq tot}}{CO_2 \text{ eq tot } g} * 100$$

Koldioxid

Metan

Dikväveoxid

Energiinsats, biogasanläggning (inkl. uppgradering)

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